



*From lab to production,  
providing a window into the process*



# The ViscoSensor On-Line Rheometer

Operation and Calculations

# Direct MFR (Constant Stress) Mode

(System Run Under Pressure Control)

**Melt Flow Rate (g/10 min.) =**

$$MFR = 10 V S d (C) \left[ \frac{2.0955 \text{ mm}}{D_c} \right]^3$$

**Where:**

V=Pump volume (cc/rev)

S=Pump speed (rpm)

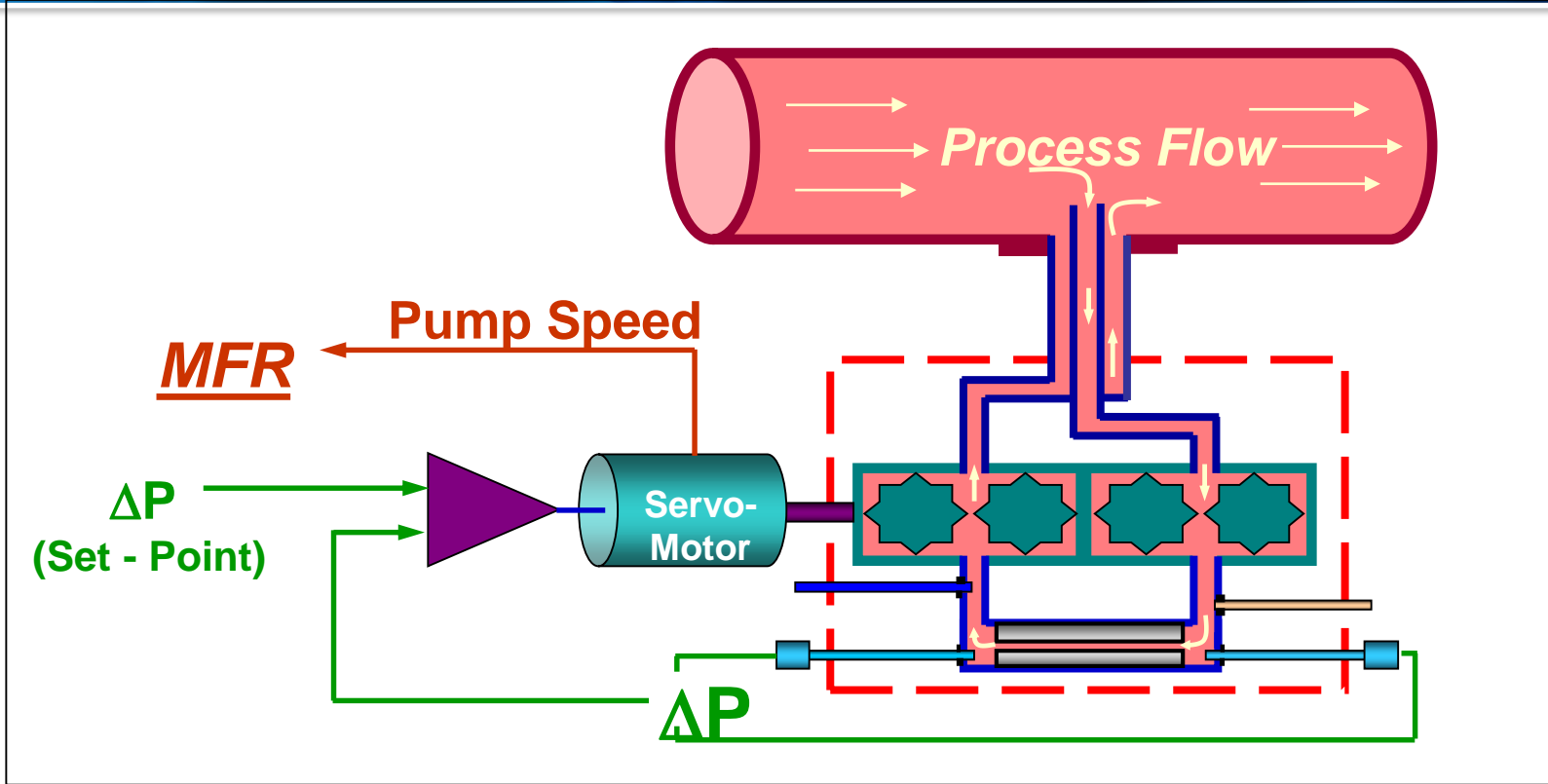
d=Polymer melt density (g/cc)

D<sub>c</sub>=Capillary diameter used (mm)

C=Correlation factor

# Direct MFR (Constant Stress) Mode

ViscoSensor Configuration for Operation Under Pressure Control



# Direct MFR (Constant Stress) Mode – Part 1

**The melt pump is run at a speed sufficient to keep a constant pressure drop across the capillary die.**

$\Delta P$  defined by conditions specified in ASTM D-1238.

$\Delta P$  is calculated from the expression:  $\Delta P = 4 \tau_{w,ASTM} (L_c / D_c)$

Where  $\tau_{w,ASTM}$  = Shear stress generated in the ASTM test.

\*For the standard ASTM Test,  $D = 2.0955$  mm and  $L/D = 3.818$ , the pressure generated by a 2.16 Kg load = 43.25 psi.

\*In the ViscoSensor when, for example,  $D = 2.0$  mm and  $L/D = 15$  the pressure drop required to simulate a 2.16 Kg load = 169.9 psi.

# Direct MFR (Constant Stress) Mode – Part 2

The RPM of the pump (S), required to maintain the correct pressure drop, the pump cc flow / rev (V), the die diameter (D) in mm, and the polymer melt density (d) at the test temperature (g/cc) are used to calculate the melt flow rate from:

Example:

$$MFR = 10 V S d (C) \left[ \frac{2.0955 \text{ mm}}{D_c} \right]^3$$

When V= 0.3 cc/rev, D<sub>c</sub>= 2.0 mm, d = 0.76 g/cc and a pump speed of 7.43 rpm is required to maintain a pressure of 169.9 psi:

$$\underline{MFR} = 10(0.3\text{cc/rev}) (7.43 \text{ rev/min})(0.76 \text{ g/cc}) (1) [2.0955 \text{ mm}/2.0 \text{ mm}]^3 =$$

19.48 g/10 min.

# Direct MFR (Constant Stress) Mode – Part 3

**C** is the correlation factor that corrects the MFR of the ViscoSensor to that measured in the laboratory.

$$C = \frac{(MFR)_{Lab}}{(MFR)_{VS}}$$

**Example:**

For the measurement shown above, if the laboratory obtains an MFR value of 18.00 g/10 min, then:

$$\underline{C} = (18.00) / (19.48) = \underline{\underline{0.924}}$$

# Viscosity (Constant Rate) Mode

(System Run Under Pump Speed Control)  
**Apparent Viscosity (Pa-s) =**

$$\eta_a = \frac{10.15 (\Delta P) D^3}{V S (L/D)}$$

Where:

V= Pump volume (cc/rev)

S= Pump speed (rpm)

$\Delta P = P_2 - P_1$  = Pressure drop  
across capillary (psi).

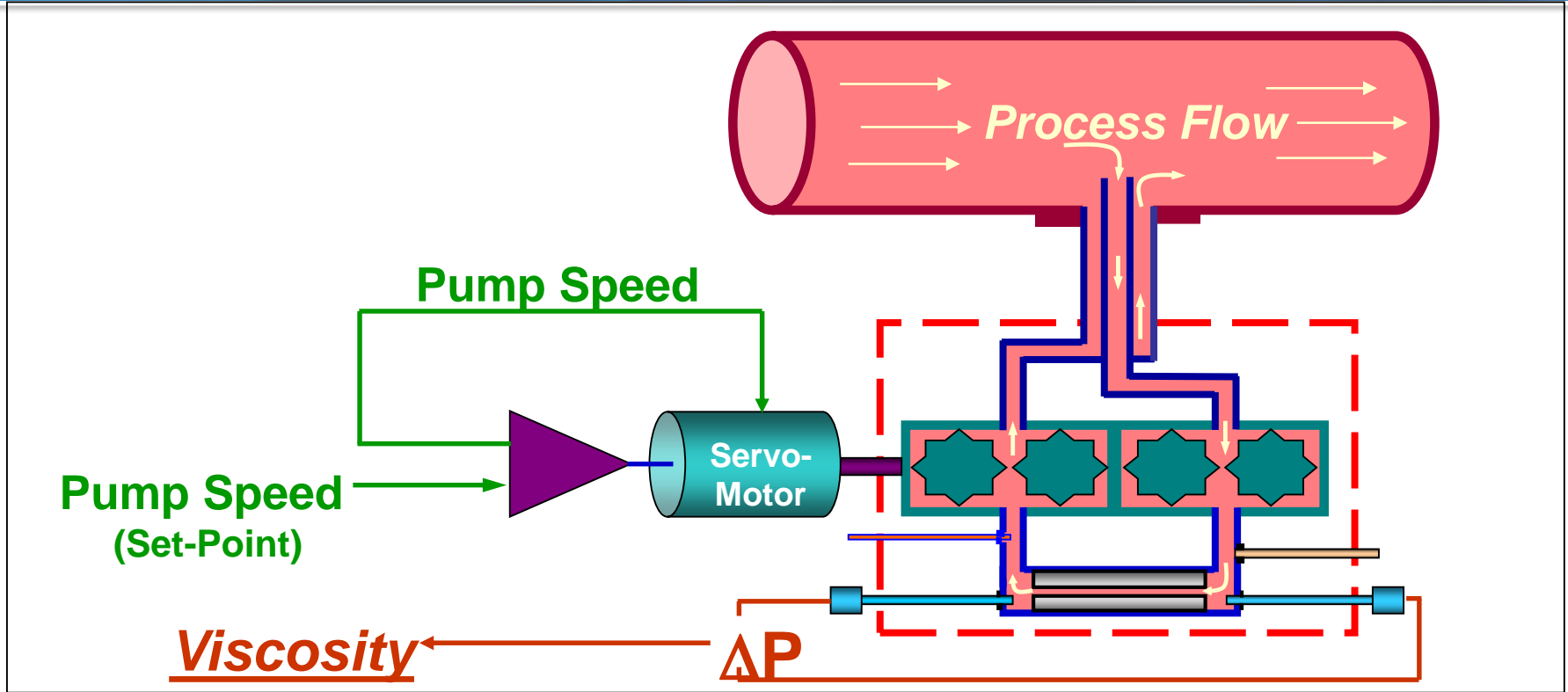
D= Capillary diameter (mm)

L= Capillary length (mm)



# Viscosity (Constant Rate) Mode

*ViscoSensor Configuration for Operation Under Pump Speed Control*



# Viscosity (Constant Rate) Mode

**The melt pump is run at a constant speed (rpm) to produce a constant shear rate.**

$$\text{Shear Rate (sec}^{-1}\text{)} = \dot{\gamma} = \frac{169.76 (V S)}{D_c^3}$$

The shear rate may be changed by changing the pump speed or the diameter (D) of the die.

**The pressure drop across the capillary is measured to determine the shear stress.**

$$\text{Shear Stress (Pa)} = \tau_w = \frac{\Delta P D_c}{4 L_c} = \frac{1723.69 (\Delta P)}{(L_c / D_c)}$$

**The apparent viscosity is determined by dividing the shear stress by the shear rate.**

$$\text{Viscosity (Pa-s)} = \eta_a = \frac{\tau_w}{\dot{\gamma}} = \frac{10.15 (\Delta P) D_c^3}{V S (L_c / D_c)}$$

# Viscosity (Constant Rate) Mode

## Example Calculation:

When: Pump Volume  $V = 0.3$  cc / rev

Die Diameter  $D = 2.0$  mm

Die Length  $L = 30.0$  mm

and operating the pump at a rate of 30 rpm produces a  $\Delta P$  of 550 psi,

then:

$$\underline{\text{Shear Rate}} = 169.76(0.3)(30) / (2)^3 = \underline{191 \text{ sec}^{-1}}$$

$$\underline{\text{Shear Stress}} = 1723.69 (550) / (30 / 2) = \underline{63202 \text{ Pa}}$$

$$\underline{\text{Viscosity}} = 10.15(550)(2)^3 / (0.3)(30)(30/2) = \underline{331 \text{ Pa-s}}$$